

Annual Report of the Ley Creek Sewage Treatment Plant, Onondaga County, N. Y., for the

Year 1953

Author(s): Uhl T. Mann

Source: Sewage and Industrial Wastes, Vol. 27, No. 12 (Dec., 1955), pp. 1418-1420

Published by: Water Environment Federation

Stable URL: http://www.jstor.org/stable/25032957

Accessed: 28-03-2018 14:55 UTC

JSTOR is a not-for-profit service that helps scholars, researchers, and students discover, use, and build upon a wide range of content in a trusted digital archive. We use information technology and tools to increase productivity and facilitate new forms of scholarship. For more information about JSTOR, please contact support@jstor.org.

Your use of the JSTOR archive indicates your acceptance of the Terms & Conditions of Use, available at http://about.jstor.org/terms



 $Water\ Environment\ Federation$  is collaborating with JSTOR to digitize, preserve and extend access to  $Sewage\ and\ Industrial\ Wastes$ 

### Operating Personnel

In 1954, four new men were placed on the staff and required training. Two men replaced staff losses due to a death and a retirement. An additional operator and a mechanic's helper were necessary through a reduction in the work week from 44 hr. to 40 hr. The operating staff now consists of two mechanics and helpers, five utility men and six operators including a relief operator. Supervision is supplied by an engineer and a chemist.

For the preceding 8 years there had been no turnover of personnel. Each operator is given an opportunity to attend the short school and various operators' meetings on a rotation basis.

Personnel worked the following distribution of hours as listed on top of second column.

In addition to the work at the treatment plant, the operating staff put in 1,162 hr. in 1953 and 1,698 hr. the following year in outside or off-site work of a maintenance nature for the city.

#### Salaries

Salaries are set by the Finance Committee of the city's council. Wages constitute 65 to 68 per cent of the total operating cost. Due to the inauguration of the 40 hr. week on Jan. 1, 1954 this budgetary item increased from \$62,933.83 to \$70,956.00. Another

	Hours	
Item	1953	1954
Sewers	1,030	1,036
Pumping stations:		
No. 1	1,923	1,712
No. 2	441	504
No. 3	381	384
Chlorination	147	115
Channels and pipe gallery	81	81
Comminutors	143	215
Grit removal	1,280	1,779
Clarifiers	6,640	5,278
Digesters	3,971	4,614
Drying beds	2,560	1,815
Building maintenance	3,764	4,681
Ground maintenance	1,345	1,397
Equipment maintenance	1,876	2,899
Adm. and laboratory	4,934	4,931
_		
Total	31,955	31,559
Vacation		1,436
Sick Leave	342	446

benefit increase for employees was the lowering from 20 yr. to 15 yr. the number of years of service necessary to be eligible for three weeks vacation.

Present annual salary scales are:

Superintendent	\$6,938.04
Chemist	3,800.49
Mechanic	4,223.16
Mechanic helper or operator	3,983.16
Utility man	3,863.16

In addition to two weeks annual vacation, 12 days per year sick leave is received and cumulative to 120 days. Surgical and hospitalization insurance is provided and all personnel are covered by social security.

# Annual Report of the Ley Creek Sewage Treatment Plant, Onondaga County, N. Y., for the Year 1953 \*

BY UHL T. MANN, Superintendent

The Ley Creek Sanitary District serves a small section of the city of Syracuse, the village of East Syracuse, several unincorporated communities and several concentrated industrial sites. Resident population of the sanitary district is estimated at 35,000, but the influx of many large industries has resulted in a population equivalent of approximately 100,000.

Originally constructed as a public works project in the period 1935-40, the 4.5 m.g.d. activated sludge plant

<sup>\*</sup>Winner of the Hatfield Award, 1954, Class II for sewage treatment plants serving populations of 10,000 to 100,000.

replaced six small sewage treatment plants. The small volume of flow in Ley Creek requires a high degree of treatment. By 1945, the treatment facilities were badly overloaded, necessitating enlargement to 9 m.g.d. in 1951.

Treatment units consist of screens, grit chambers, pre-aeration tanks, primary settling and aeration units. Separate sludge digestion is followed by sludge drying on either vacuum filters or drying beds. Sludge gas is stored in a 15,000 cu. ft. gas holder and

a 40,000 cu. ft. digester. Chlorination of the plant effluent is practiced during the months of May through September.

Present facilities provide pumping capacity for 40 m.g.d., primary treatment for 20 m.g.d. and standard rate activated sludge treatment for 9 m.g.d. Soil conditions at the plant site require the operation of a dewatering system to lower the ground water and eliminate danger of the tanks floating when emptied. Part of this system is used for process water.

TABLE II.—Summary of 1953 Operating Data, Ley Creek (N. Y.) Sewage Treatment Plant

Item	Average	Item	Average
Rainfall (in.)	29.72	D.O., aeration tank (p.p.m.)	2.8
Population:		Excess activated sludge (cu. ft.	
Connected (estimated)	35,000	per m.g.)	2,530
Equiv., B.O.D	135,000	Chlorination:	
Equiv., susp. sol	81,500	Days	137
Sewage flow (m.g.d.)	5.91	Lb. per day	525
Screenings (cu. ft. per m.g.)	4.2	Residual (p.p.m.)	0.59
Grit (cu. ft. per m.g.)	6.75	Raw sludge:	
pH:		Pumped per day (cu. ft.)	4,420
Influent	7.36	pH	6.11
Settled	7.43	Dry solids (%)	4.6
Final effl	7.59	Volatile solids (%)	72
Settleable solids:		Digested sludge:	
Influent (ml. per liter)	10.1	To drying beds (cu. ft. per day)	3,062
Primary effl. (ml. per liter)	1.4	pH	7.46
Reduction (%)	87	Dry solids (%)	4.4
Suspended solids:		Volatile solids (%)	52
Influent (p.p.m.)	314	Gas production:	
Primary effl. (p.p.m.)	154	Daily average (cu. ft.)	82,242
Plain aeration effl. (p.p.m.)	71	Cu. ft. per lb. (dry) volatile sol-	·
Activated sludge effl. (p.p.m.)	19	ids added	9
Combined effl. (p.p.m.)	45	Gas analysis:	
Reduction (%)	85.5	CO <sub>2</sub> (%)	33
B.O.D., 5-day:		Power (k.w.h. per day)	3,264
Influent (p.p.m.)	459	Outlet stream analyses (p.p.m.):	ŕ
Primary effl. (p.p.m.)	310	Upstream ½ mile:	
Plain aeration effl. (p.p.m.)	166	D.O	7.6
Activated sludge effl. (p.p.m.)	24	B.O.D	14
Combined effl. (p.p.m.)	112	Susp. sol	24
Reduction (%)	75.5	Downstream ¼ mile:	
Activated sludge data:		D.O	4.6
Aeration period (hr.)	7.12	B.O.D	64
Air consumption (cu. ft. per gal.		Susp. sol	56
sewage)	1.97	Stream flow 1 (c.f.s.)	26.5
Returned sludge (% by volume)	27.6	Treatment costs (\$):	
Mixed liquor suspended solids		Plant operation1	.74,517.00
(p.p.m.)	1,862	Debt retirement3	
Sludge index	103	Per m.g. <sup>2</sup>	81.00
		Per capita <sup>2</sup>	1.74

<sup>1</sup> Includes plant effluent.

<sup>2</sup> Does not include debt retirement.

### Operation

Construction features of the plant permit operation as two separate units. During 1953, one-half of the plant was operated as a standard rate activated sludge plant while the other half was operated as a plain aeration plant. Each half of the plant received approximately one-half of the flow except when shock loads upset the activated sludge process. At these times the flow was adjusted to permit plain aeration of the larger part of the flow. The combined effluent of the two sections represented a suspended solids reduction of 85.5 per cent and a B.O.D. reduction of 75.5 per cent. Industrial plants produce 60 per cent of the B.O.D. load to the treatment plant.

The population equivalent is 135,000 when based on the B.O.D. load and 81,500 when based on the suspended solids. Daily analyses showed the strongest sewage had a B.O.D. of 800 p.p.m. The aeration units experienced B.O.D. loadings of 57 to 90 lb. per 1,000 cu. ft. of tank capacity. The overload has been calculated at 60 to 100 per cent of design capacity. On many days the primary tanks fail to provide any reduction in the B.O.D. load due to the high percentage of dissolved solids in the sewage.

The activated sludge treatment, however, remained quite constant with little change in solids, air supply, aeration time, sludge wasted or rate of returned sludge.

Reduction in the quantity of screenings (15 per cent) and scum (21 per cent) resulted in better digester operation. Digestion time was reduced, gas production per pound of volatile matter was increased and there was no lost digester capacity due to heavy scum layers. Approximately 1,100,000 cu. ft. of digested sludge was pumped; one-half to drying beds and one-half to lagoons. The vacuum filters were not operated because funds were not provided for the purchase of chemi-Almost 85 per cent of the digester gas produced was used by the blower gas engines and digester heat-The present digestion ing system. units are overloaded about 17 per cent on the basis of design.

The operation cost increase is attributed entirely to maintenance. As the equipment gets older the need for repairs and replacement increases. The operating staff numbers 27 and is responsible for the treatment plant and sanitary sewers.

The most pressing operation problems are due to industrial wastes and overloaded treatment units. Each year these conditions become more aggravated. It is difficult to control slugs of industrial wastes, although the industries have been most cooperative.

A summary of operating data for 1953 is given in Table II.

## SCALE MODEL SEWAGE TREATMENT PLANT

A scale model sewage treatment plant that actually operates has aided the citizens of San Diego, Calif. in understanding this vital municipal service. Designed and constructed under the supervision of Eric V. Quartley, Superintendent, Sewage Treatment Division, the model (Figure 1) represents many hours of diligent work by division personnel.

The model is built to a horizontal scale of approximately 1 in. to 10 ft. while the vertical scale is slightly exaggerated to permit the showing of equipment details. Measuring 5 ft. by 8 ft. in plan the unit is mounted on a sturdy table fitted with casters to facilitate moving. A wood frame glass cover protects the model when on display.